3498

Denpo *et al.* [3] actually measured the cupric ion concentration and hydrogen ion concentration distributions near vertical walls using two-wavelength holographic interferometry. The boundary layer thicknesses of the cupric ion and hydrogen ion did not show any appreciable difference. (Both were approximately 0.5 mm.)

(3) Previous studies [4, 5] indicate that the Rayleigh number is simply additive, if one buoyancy is significantly larger than the other and/or if the ratio of diffusivities is close to unity. According to Nilson and Baer [6], the counter-flow at buoyancy ratio of 0.1 and diffusivity ratio 3 falls well within the inner-dominated flow region. The fluid flow can be assumed to be in the simply-additive region [7] and a single solutal Rayleigh number can be used.

(4) The concentration increase of  $H_2SO_4$  at the cathode is approximately 35–45% of the bulk concentration of  $CuSO_4$ [8, 9]. In the present experiment, the concentration of  $CuSO_4$ is in the range of 0.015–0.05 mol 1<sup>-1</sup>, and it creates a concentration increase of  $H_2SO_4$  by 0.005–0.02 mol 1<sup>-1</sup>, which is considerably smaller than the nominal concentration of  $H_2SO_4$  in the bulk fluid (1.5 mol 1<sup>-1</sup>). The concentration variation of hydrogen ion in the cavity due to the migration effect would be between 1.48 and 1.52 mol 1<sup>-1</sup> at worst.

(5) The triply-diffusive analysis could be suggested for future studies for further refinements in the experimental technique.

HWATAIK HAN

Department of Mechanics and Design Kook Min University Seoul, Korea

Int. J. Heat Mass Transfer. Vol. 35, No. 12, p. 3498, 1992 Pergamon Press Ltd. Printed in Great Britain

## REFERENCES

- Y. Kamotani, L. W. Wang, S. Ostrach and H. D. Jiang, Experimental study of natural convection in shallow enclosures with horizontal temperature and concentration gradients, *Int. J. Heat Mass Transfer* 28, 165–173 (1985).
- A. F. W. Cole and A. R. Gordon, The diffusion of copper sulfate in aqueous solutions of sulfuric acid, *J. Phys. Chem.* 40, 733-737 (1936).
- K. Denpo, T. Okumura, Y. Fukunaka and Y. Condo, Measurement of concentration profiles of Cu<sup>2+</sup> ion and H<sup>+</sup> ion near a plane vertical cathode by two-wavelength holographic interferometry, J. Electrochem. Soc. 132, 1145-1150 (1985).
- 4. E. V. Somers. Theoretical considerations of combined thermal and mass transfer from a vertical flat plate, *J. Appl. Mech.* 23, 295-301 (1951).
- 5. F. A. Bottemanne, Experimental results of pure and simultaneous heat and mass transfer by free convection about a vertical cylinder for Pr = 0.71 and Sc = 0.63, *Appl. Scient. Res.* **25**, 372-382 (1972).
- R. H. Nilson and M. R. Baer, Double-diffusive counterbuoyant boundary layer in laminar natural convection, *Int. J. Heat Mass Transfer* 25, 285–287 (1982).
- H. Han and T. H. Kuehn, Double diffusive natural convection in a vertical rectangular enclosure—II. Numerical study, *Int. J. Heat Mass Transfer* 34, 461-471 (1991).
- 8. C. R. Wilke, M. Eisenberg and C. W. Tobias, Correlation of limiting currents under free convection conditions, *J. Electrochem. Soc.* **100**, 513–523 (1953).
- J. R. Selman and J. Newman, Free-convection mass transfer with a supporting electrolyte, *J. Electrochem. Soc.* 118, 1070–1078 (1971).

## Comments on "Coupled heat and mass transfer by natural convection from vertical surfaces in porous media"

I AM VERY pleased that this new full-length paper [1] confirms our scale-analysis predictions and extends the range covered by our similarity solutions [2]. However, there is one erroneous claim in this new paper, and I must correct it.

On page 1192, the authors state that "Contrary to what has been reported by Bejan and Khair (ref. [2] below), we have found ... that solutions in the range of N < -1 are impossible." In other words, the solutions reported by us [2] for the negative buoyancy ratios  $-5 \le N \le -1$  are fictitious. They explain this claim in the footnote: "Although Bejan and Khair did not state clearly in their paper, the solutions they presented for the range  $-5 \le N \le -1$  actually corresponded to a different problem, for which the convective flow is always downward, such that the parallel double boundary-layer structure is maintained."

Lai and Kulacki are wrong. I draw attention to page 913 in our paper [2] in which we pointed out that: "The only change that occurs when N is negative and large in absolute value is that the double boundary layers sketched in (our) Figs. 1 and 2 develop in the negative y direction, since the flow will then be downward." Obviously, our solutions for  $-5 \le N \le -1$  are correct, and we explained their physical meaning quite clearly.

Recognition of the possibility of two flow directions, or the condensation of two problems into a unified treatment (for brevity, among other virtues) was one of the central ideas of our paper. We emphasized this by using |N| instead of N, wherever appropriate. In our drawing of the double boundary layer structure (Fig. 2) we did not indicate 'up' or 'down': note that y, the y arrow and the gravity vector are missing.

As an aside, I note that Lai and Kulacki did not mention ref. [3], which is where this problem was first formulated and solved by scale analysis.

## Adrian Bejan

J. A. Jones Professor of Mechanical Engineering Duke University Durham, NC 27706, U.S.A.

## REFERENCES

- F. C. Lai and F. A. Kulacki, Coupled heat and mass transfer by natural convection from vertical surfaces in porous media, *Int. J. Heat Mass Transfer* 34, 1189–1194 (1991).
- A. Bejan and K. R. Khair, Heat and mass transfer by natural convection in a porous medium. *Int. J. Heat Mass Transfer* 28, 909–918 (1985).
- A. Bejan, Convection Heat Transfer, pp. 335-338. Wiley, New York (1984).